

Reynolds number similarity of orthogonal decomposition of the outer layer of turbulent wall flow

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Experimental evidence is presented to show that in the outer region of wall-bounded turbulent flow both the eigenfunctions and the eigenvalue spectra of the one-dimensional proper orthogonal decomposition have forms that are independent of Reynolds number when scaled by the wall friction velocity and the outer length scale.

The proper orthogonal decomposition of Lumley^{1,2} defines a deterministic set of orthonormal basis functions for a given random process. The set is optimal in the sense that expansion in terms of these basis functions converges faster than expansion in terms of any other set of basis functions. The topic has been reviewed recently by Berkooz, Holmes and Lumley³. When applied to turbulent velocity fields, the basis functions are the eigenfunctions of a Fredholm integral equation whose kernel is the two-point correlation function of the random velocity field. If the turbulence is statistically homogeneous, the eigenfunctions reduce to the trigonometric functions and POD becomes conventional Fourier analysis. If, however, the turbulence is statistically inhomogeneous, POD defines a non-trigonometric set of eigenfunctions whose structure reflects the physics of the inhomogeneity, as imbedded in the structure of the two-point correlation function.

While many of the more attractive properties of POD derive from the fact that it is based on correlation functions that contain important information about the physics of a particular flow, the need to input the correlation functions also makes implementation of the POD difficult because the correlation functions are seldom available, especially for inhomogeneous, anisotropic flow. There are two scenarios in which this difficulty is ameliorated.

First, if the eigenfunctions of the POD are sufficiently insensitive to the form of the correlation function, it may be satisfactory to use approximate correlation functions, or approximate eigenfunctions which, though incorrect, capture at least some of the important aspects of the flow inhomogeneity. The work of Sirovich and Rodriguez⁴ and Rodriguez and Sirovich⁵ with the POD of the Ginzburg-Landau equation suggests that this may be

possible. They considered expansion of the solution at one value of a Reynolds number-like parameter that was based on eigenfunctions computed from the correlation function for a value of the parameter that differed by a factor of three. The eigenfunctions for the first Reynolds number, were effectively sub-optimal models of the eigenfunctions for the second Reynolds number. Expansion in terms of the sub-optimal eigenfunctions converged almost as fast as the optimal expansion.

Second, if the eigenfunctions possess a property of universality similar, for example, to that of the celebrated law of the wall or the spectral similarity laws of turbulence, then it would be possible to use a single set of eigenfunctions to represent flows at many Reynolds numbers. The work of Chambers, et al.⁶ explored this possibility by using Burger's model on a unit interval with the random forcing to create a temporally stationary, spatially inhomogeneous process possessing a two-scale boundary layer character at the end-points of the interval. They showed that the POD eigenfunctions in the inhomogeneous spatial variable were similar over a range of Reynolds numbers if they were scaled on outer variables. It was conjectured that the POD of real turbulence might also obey such a generalized law of Reynolds number similarity.

In this letter, we describe results that indicate that the one-dimensional eigenfunctions of three dimensional wall turbulence exhibit similarity in the form of Reynolds number independence of the outer regions of both the eigenfunctions and the spectrum of eigenvalues, when scaled properly with outer variables. Demonstration of this property is based on experiments conducted in plane, fully developed turbulent channel flow at two Reynolds numbers, $Re_h = Ubh/\nu = 5,378$ and $29,935$, where U_b is the bulk velocity, $2h$ is the total channel height, and ν is the kinematic viscosity. These two Reynolds numbers provide a range of variation (5.5:1) adequate to make a credible test of Reynolds number invariance while keeping the lower Reynolds number high enough to avoid some of the peculiarities of very low Reynolds number turbulence, and the upper Reynolds number low enough to maintain reasonable spatial resolution of the outer scales of motion.

The rectangular channel cross-section is 609.6 mm wide by $2h=48.75$ mm high and the water flow is fully developed. Conventional coordinates are used with $(u,v,w)=(u_1,u_2,u_3)$ referred to (x,y,z) coordinates in the streamwise, cross-stream and spanwise directions, respectively. Turbulent flow in this channel has been documented previously by LDV studies^{7,8}, and comparisons of the time averaged moments of the u - and v - fluctuations through fourth order at $Re_h=2,777$ and $18,000$ agree well with the channel flow results of other investigators. Pertinent properties of the flows are listed in Table 1, wherein u^* is the friction velocity found by using direct measurements of the bulk velocity and Dean's correlation of the friction coefficient as explained in Ref. 8.

Table 1. Properties of channel flows

$U_b h/\nu$	U_b (mm/s)	u^* (mm/s)	ν/u^* (mm)	Δx^+	Δy^+	Δz^+
5,378	212	12.4	0.0775	20.6	10.3	10.3
29,935	1,074	50.7	0.0172	93.0	46.5	46.5

$\Delta x/h$	$\Delta y/h$	$\Delta z/h$
0.065	0.032	0.032

Measurement of the u - and v -components of the velocity field in an x - y plane extending completely across the channel are made by planar light sheet particle image velocimetry. The techniques have been described previously in Liu, et al.⁹ Scattering particles were 9.5 micron nominal mean diameter aluminum oxide particles illuminated by two 2J ruby laser pulses. The time between pulses was adjusted to produce an average displacement of approximately 0.25 mm, thereby satisfying the "one-quarter rule" for double-pulsed autocorrelation PIV¹⁰. Double pulsed particle images over a field of view that spanned the channel and covered approximately 120mm in the streamwise direction were recorded on 4" x 5" Kodak 4415 film using a single lens scientific camera with magnification $M=0.97$ and $f/9$ Schneider lens. The angular field-of-view was small enough to limit errors due to the perspective effect¹¹ to a maximum value of 1.7 % of the bulk velocity over the entire field of view. Photographs were interrogated automatically by direct spatial correlation of the images in small interrogation spots using the PIV interrogation system described in Ref. 12.

The measurements so obtained represent the Eulerian velocity averaged over a measurement volume defined by the virtual intersection of the interrogation spot with the laser light sheet¹³. The interrogation spot dimensions were chosen to produce measurement volumes with dimensions $\Delta x= 1.6\text{mm}$, $\Delta y=0.8\text{ mm}$ and $\Delta z= 0.8\text{mm}$ in the fluid. The dimensions in Table 1 are given in terms of viscous wall unit and relative to the channel height. At the lower Reynolds number the spatial resolution is comparable to that achieved in direct numerical simulations, but at the higher Reynolds number the measurement from each independent (e.g. non-overlapping) interrogation spot represents an average over a significant range of small scales. For example, the resolution in the y -direction $\Delta y^+= 46.5$ is inadequate to resolve the buffer layer, but relative to the outer length scale h , the resolution $\Delta y/h=0.032$ is capable of resolving POD modes in the y -direction up to mode numbers of order 15, considerably beyond the mode number considered here. Interrogation

was performed on a uniform, rectangular grid of points with spacing 1.2mm in the x - and 0.6mm in the y -- directions (25% overlap of interrogation spots).

Statistical quantities are computed by averaging along line of constant y in the data from each PIV photograph, and averaging the line averages over ensembles of 60-80 photographs for each Reynolds number. Turbulent fluctuation data is defined by subtracting the ensemble mean velocity from the total velocity field of each photograph. Profiles of the mean streamwise velocity, the *rms* streamwise and cross-stream turbulent velocities and the turbulent Reynolds shear stress all compare well with accepted data.

The two-point spatial correlation function with one-dimensional separation in the y -direction

$$R_{ij}(y, y') = \langle u_i(x, y, z, t) u_j(x, y', z, t) \rangle, \quad i, j = u, v \quad (1)$$

is computed from the ensemble of PIV photographs in a similar manner. To illustrate the character of the PIV correlation data normalized correlation coefficients

$$R_{uu}(y, y') / [R_{uu}(y, y) R_{uu}(y', y')]^{1/2}$$

are plotted in Fig. 1 for three different values of y . The complete data set for one Reynolds number consists of 75 such curves, one for each y -location across the width of the channel. Similar data are available for R_{vv} , R_{uv} and R_{vu} . Near the top of the channel laser flare made PIV measurements unreliable.

The one- dimensional POD is found by solving the eigenvalue problem

$$\int_0^h R_{ij}(y, y') \varphi_j^{(n)}(y') dy' = \lambda_n \varphi_i^{(n)}(y) \quad (2)$$

The decomposition is performed on the half-channel domain $(0, h)$, principally to avoid the region of missing correlation data on the upper wall, but also because the half-channel velocity profile corresponds more closely to a boundary layer than the full channel profile. Integration is done using the trapezoidal rule and the IMSL eigenvalue routine DEVCHF. Computations are carried out up to order $n=10$. Beyond that order statistical sampling errors in the measurement of R_{ij} render the eigenvalue computation unreliable.

The scales of motion in the outer layer of the channel flow are taken to be h and u^* . In terms of these scales the non-dimensional length is y/h , the non dimensional eigenvalue is $\lambda \mu^{*2} h$, and the non-dimensional eigenfunctions are $h^{1/2} \varphi_i^{(n)}$. The factor of

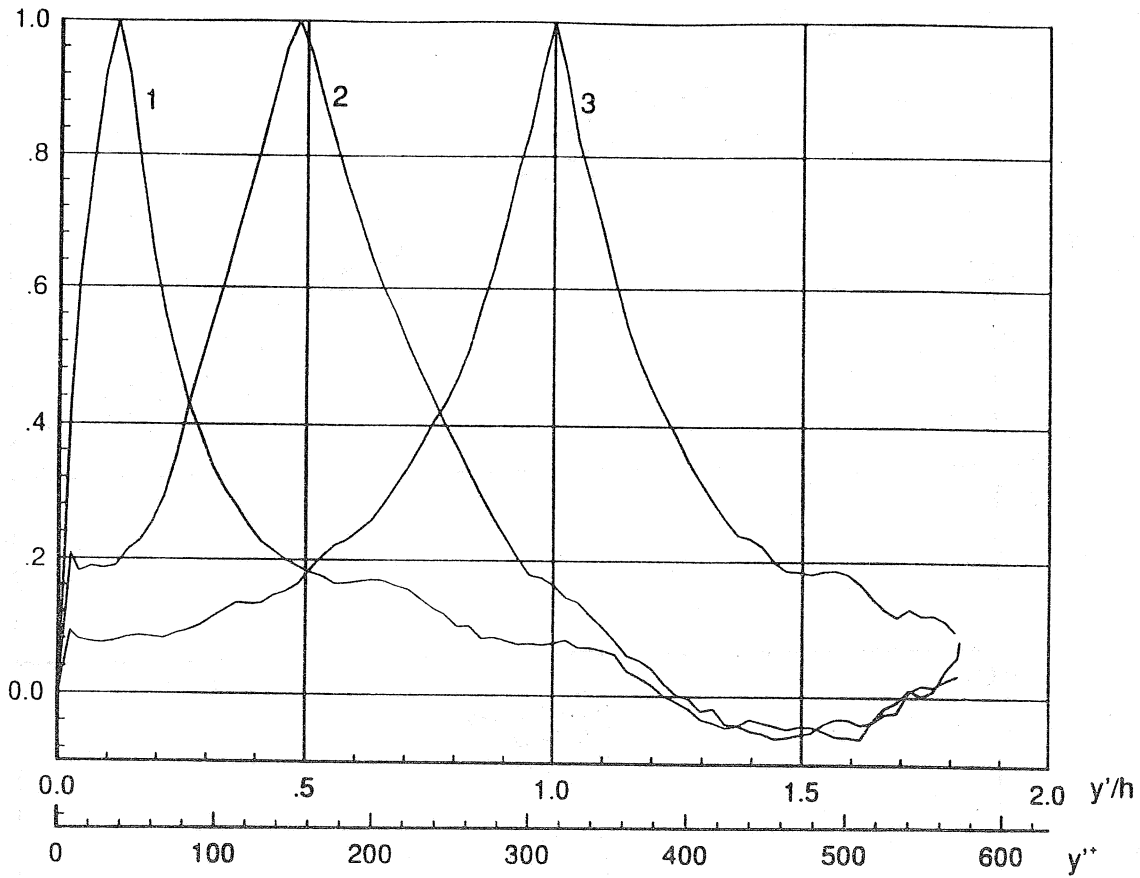


FIG. 1. Two-point correlation functions $R_{uu}(y, y') / u_{rms}(y) u_{rms}(y')$ at $Re_h = 5,378$. The fixed points are at $y/h = 0.114, 0.476$, and 0.50 , corresponding to the top of the buffer layer, the top of the log-layer, and the centerline of the channel.

$h^{1/2}$ is determined by the condition of orthogonality⁶

$$\int_0^h \varphi^{(m)}(y) \varphi^{(n)}(y) dy = \delta_{mn}, \quad (3)$$

The scaling of $\varphi_i^{(n)}$ is independent of u^* because Eq.(2) is homogeneous in $\varphi_i^{(n)}$, and it therefore imposes no dimension on the eigenfunction.

Non-dimensional eigenfunctions computed from the correlation data at $Re_h = 5,378$ and $29,935$ are compared in Fig. 2. (Scaling by $h^{1/2}$ is optional in Fig. 2 because the channel height was not varied in the experiments. It is introduced solely for consistency.) Eigenfunctions of the u - and v - components are shown through order four. The u -eigenfunctions are clearly dependent on the Reynolds number in the region adjacent to the wall where the inner wall layer significantly retards the streamwise motion. This region extends up to approximately $y/h = 0.2$ depending upon the Reynolds number. Above the

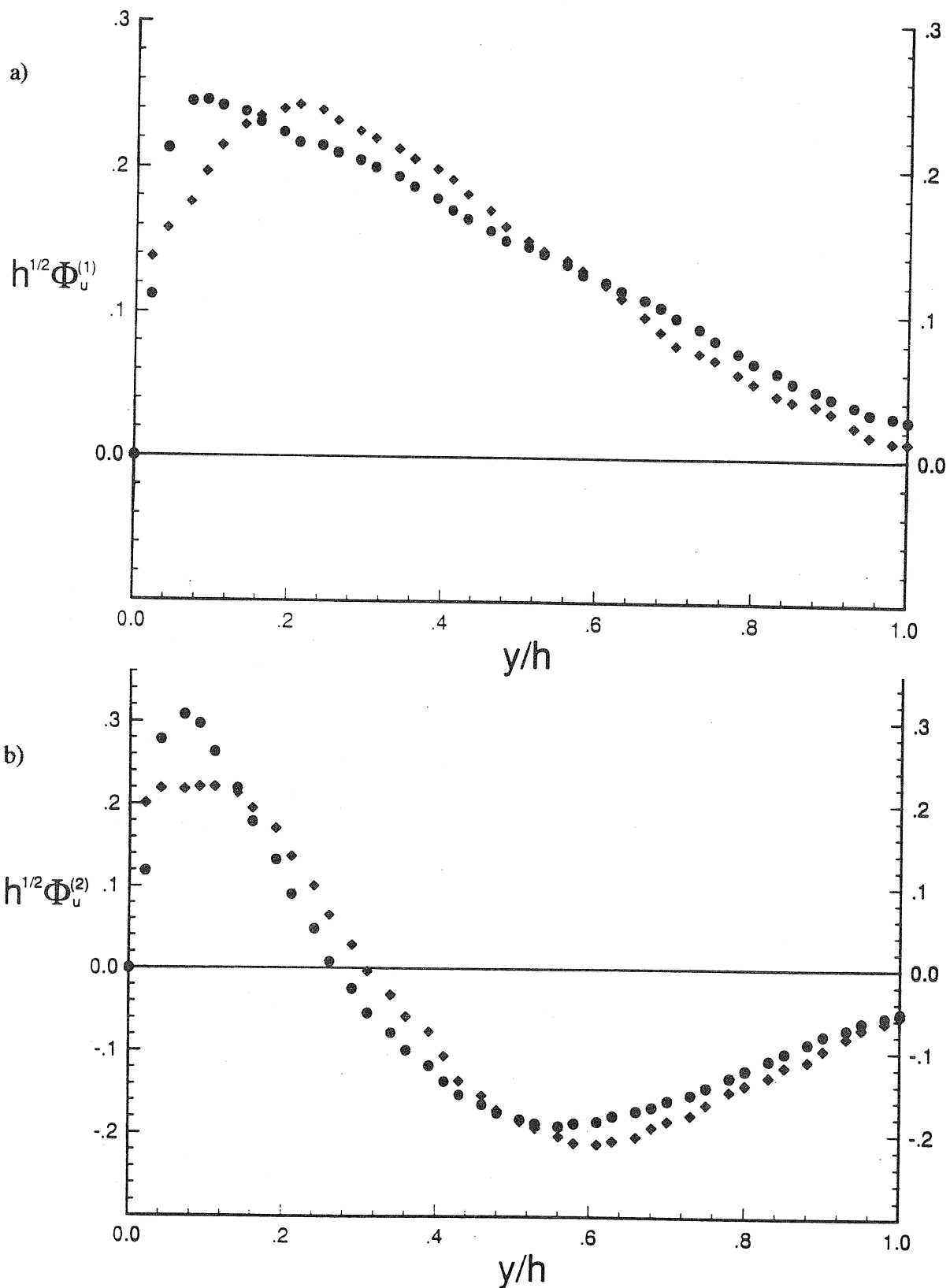


FIG. 2. Eigenfunctions of the 1-D POD of turbulent channel flow at Reynolds number=5,378 (circles), 29,935 (squares). The decomposition domain is $0 \leq y \leq h$. (a), (b), (c), and (d) are the eigenfunctions of the u -component, $n=1, 2, 3, 4$; (e), (f), (g), and (h) are the eigenfunctions of the v -component, $n=1, 2, 3, 4$.

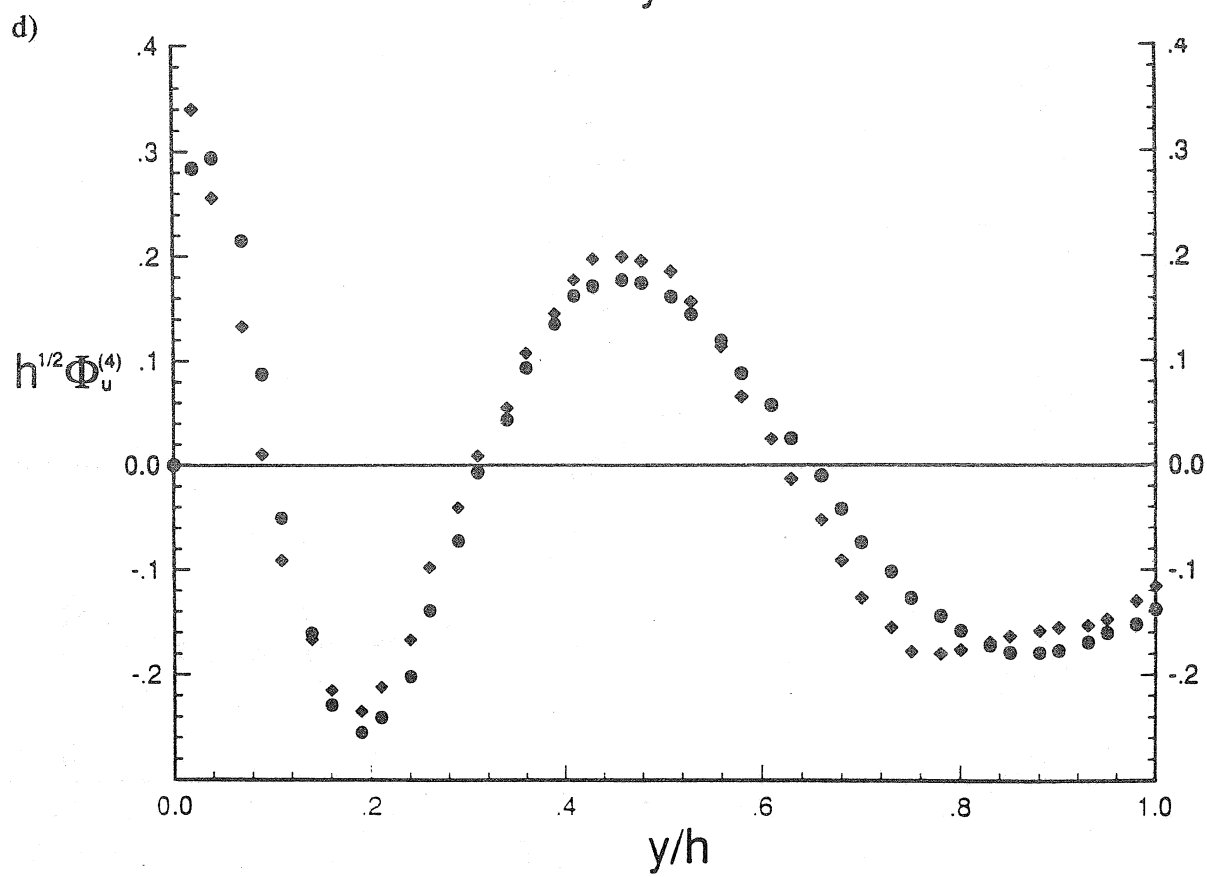
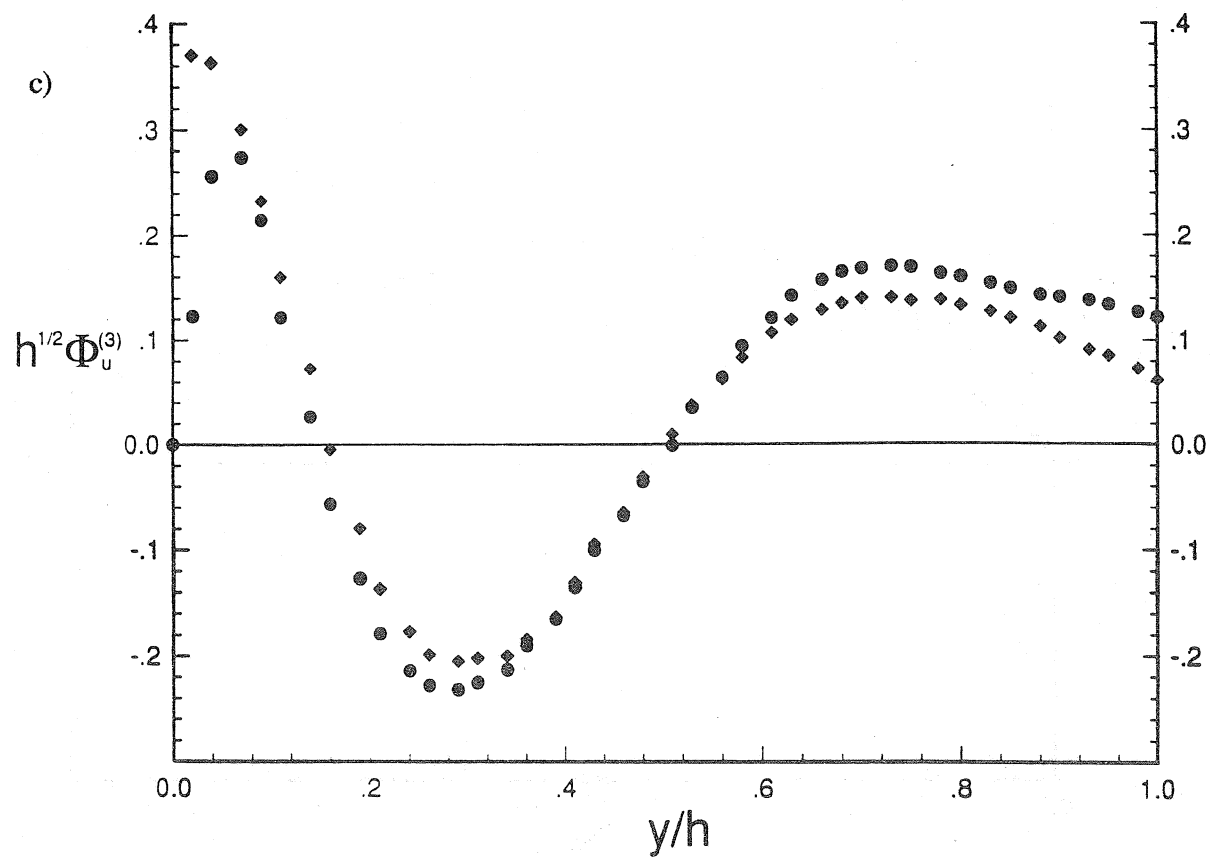


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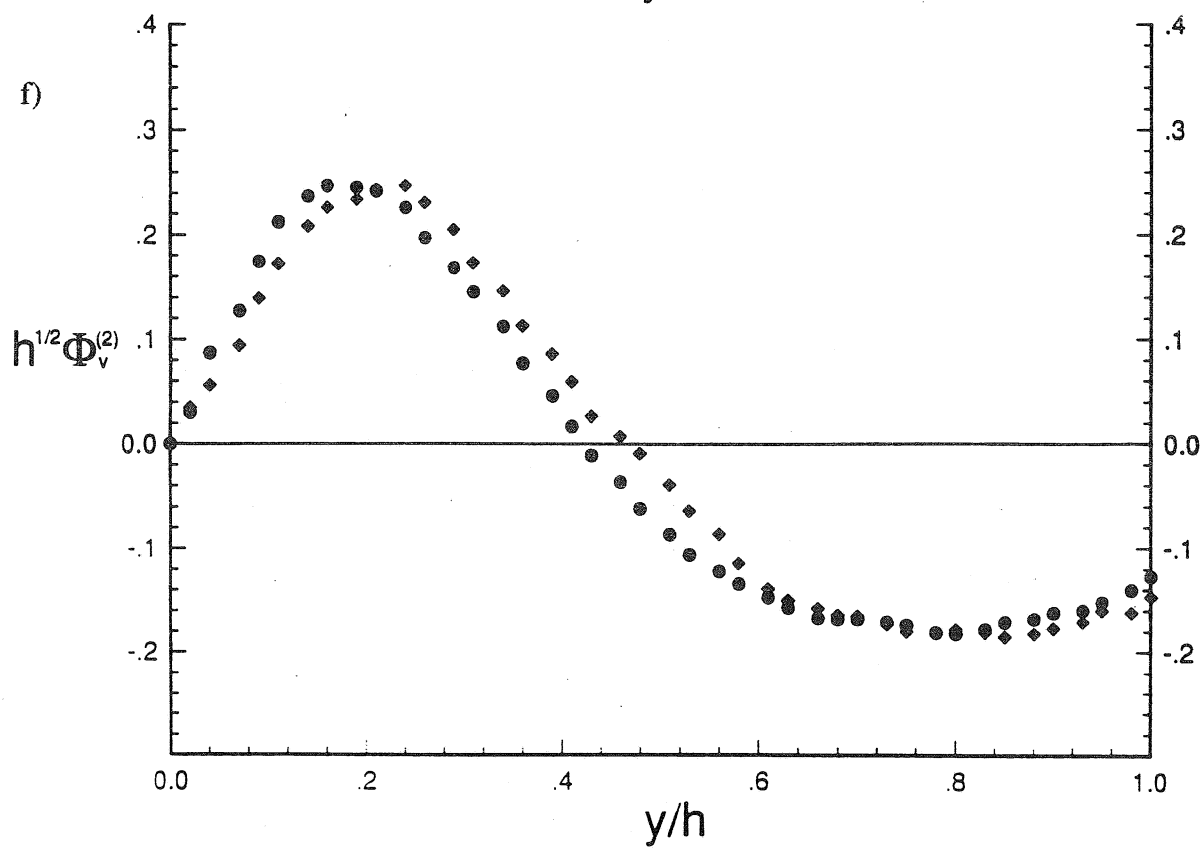
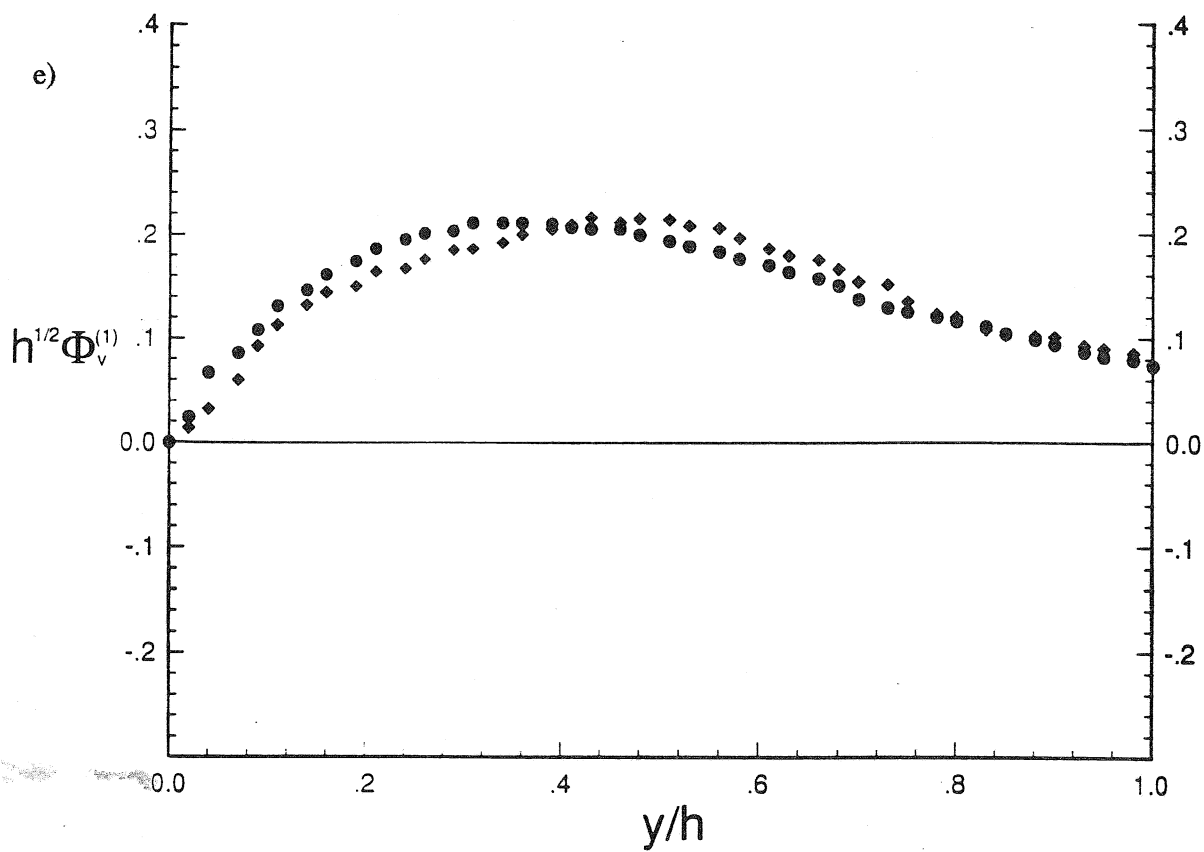


FIG. 2. Continued

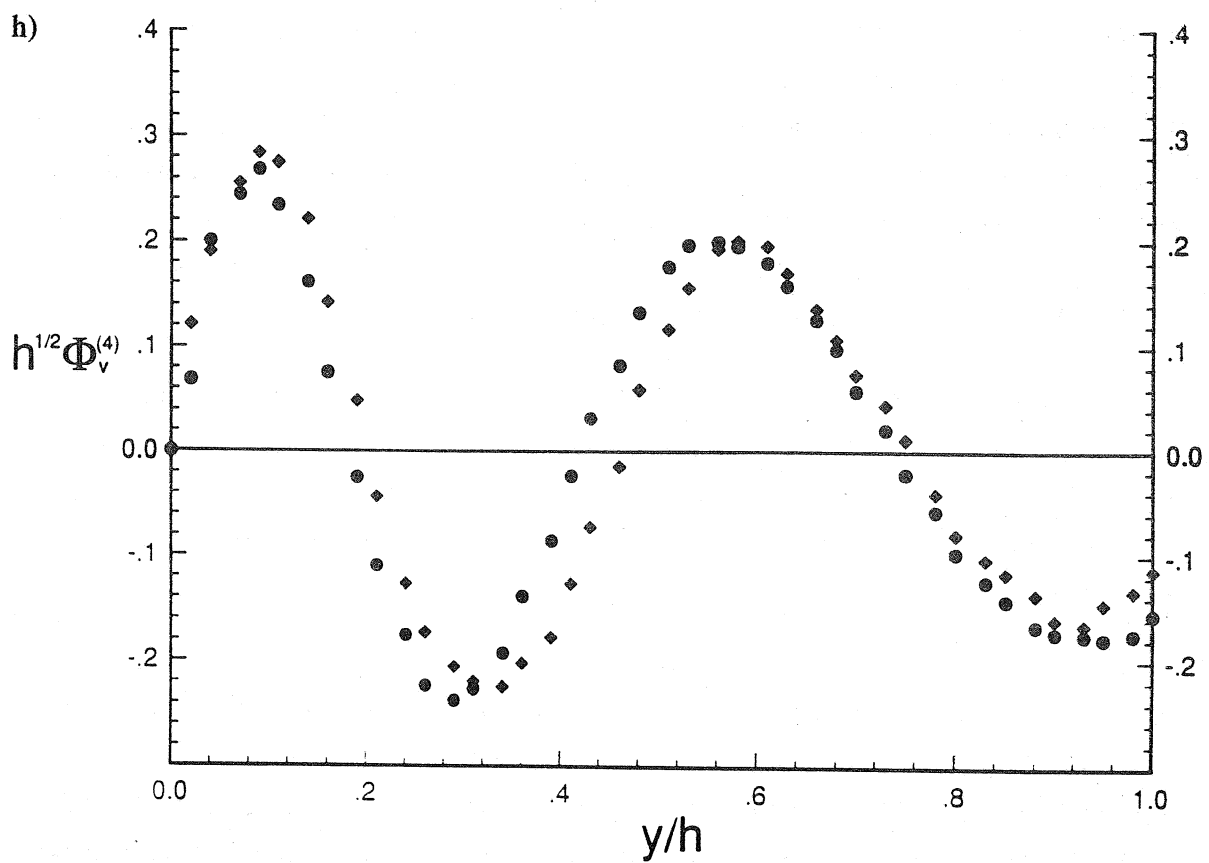
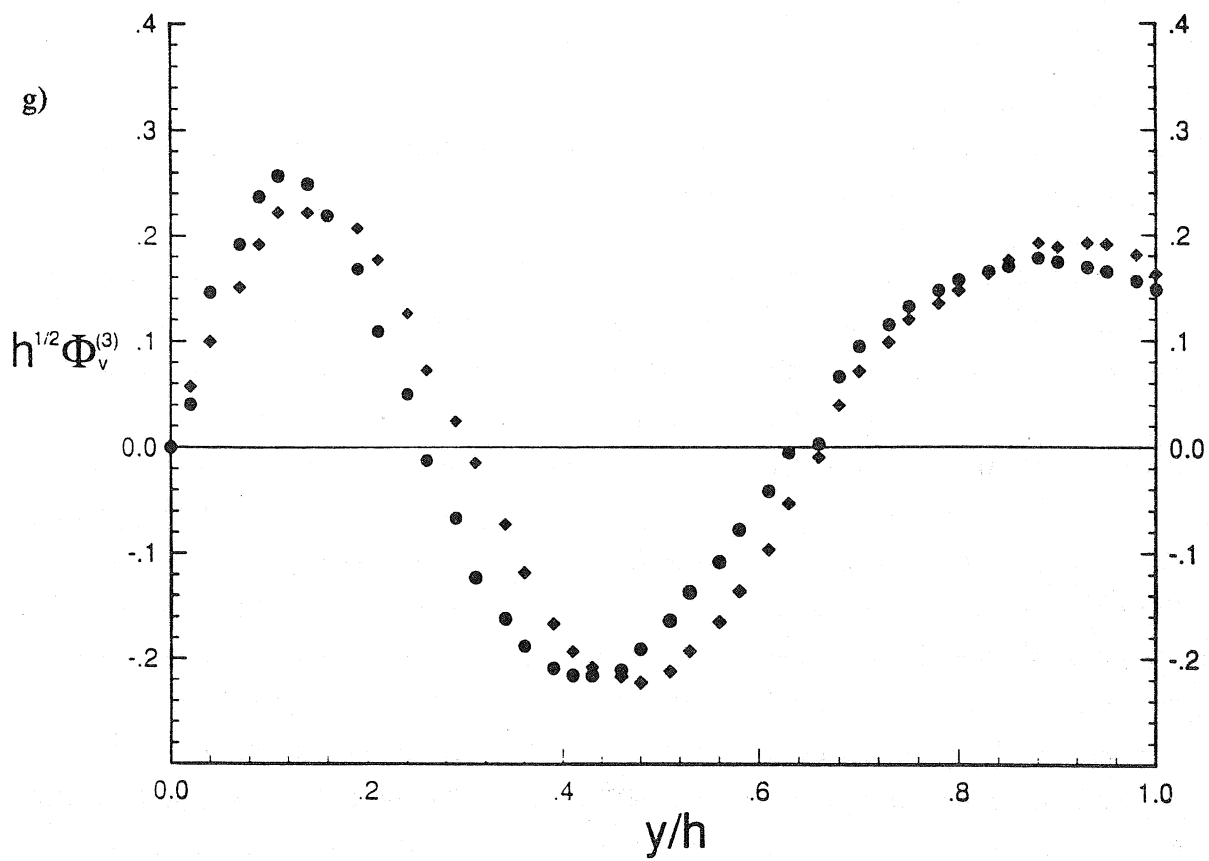


FIG. 2. Continued

wall layer the eigenfunctions of any order are remarkably similar at both Reynolds numbers. Small differences that do appear in the comparisons are within the estimated sampling error in the measurements of R_{ij}

The non-dimensional eigenvalue spectra of the POD for both Reynolds numbers are shown in Fig. 3. Since the spectra are monotonic, the mode number n of the energy-ordered eigenvalues is related simply to the *sequency*, which is defined as the number of zero crossings of the associated eigenfunction in the interior of the domain $(0, h)$. By inspection of Fig. 2 it is clear that the mode number is equal to the number of half-cycles in the length h . If the process was homogeneous, the eigenfunctions would be trigonometric, and the lengths of the cycles would be uniform. Since it is inhomogeneous, the lengths of the cycles vary, increasing with distance from the wall. Evenso, the analogy with trigonometric functions is clear, and it is natural to interpret n as the number of half-wavelengths in h . To within a factor of 2π this is analogous to the usual trigonometric wavenumber k made dimensionless by the outer scale of length, h . Thus, Fig. 3 represents the outer scaling of the eigenvalue spectrum. The similarity of the spectra at the different Reynolds numbers is evident. It was shown earlier that spectra of Burgers equation which were similar at low mode numbers still depended upon the Reynolds number at higher values of the mode number, presumably because of the increased significance of viscosity at small scales. The spectra for the channel show no such differences, suggesting that the mode numbers attainable from the experimental data are not high enough to reveal clearly the effects of viscosity on the spectra. On physical grounds and by analogy with the similarity behavior of power spectra of homogeneous turbulence we should not expect the Reynolds number similarity to extend over all mode numbers.

The foregoing results lead us to state the following principle of large scale similarity of the POD eigenfunctions for a fully turbulent process: *In the region outside of the wall layer and in the range of sequencies where the wavelength is large compared to the wall layer viscous length scale, both the eigenfunctions and the spectrum of the eigenvalues when scaled by outer layer variables are independent of the Reynolds number for sufficiently large Reynolds number.*

It is of considerable interest to ask if the similarity principle can be extended from channel flow to a broader class of turbulent wall flows. Some indication that such generalization is possible is obtained by comparing the POD results of Lu and Smith¹⁴ for a boundary layer to the present results for channel flow. The Reynolds numbers of these flows based on the centerline velocity and the momentum thickness of the mean velocity

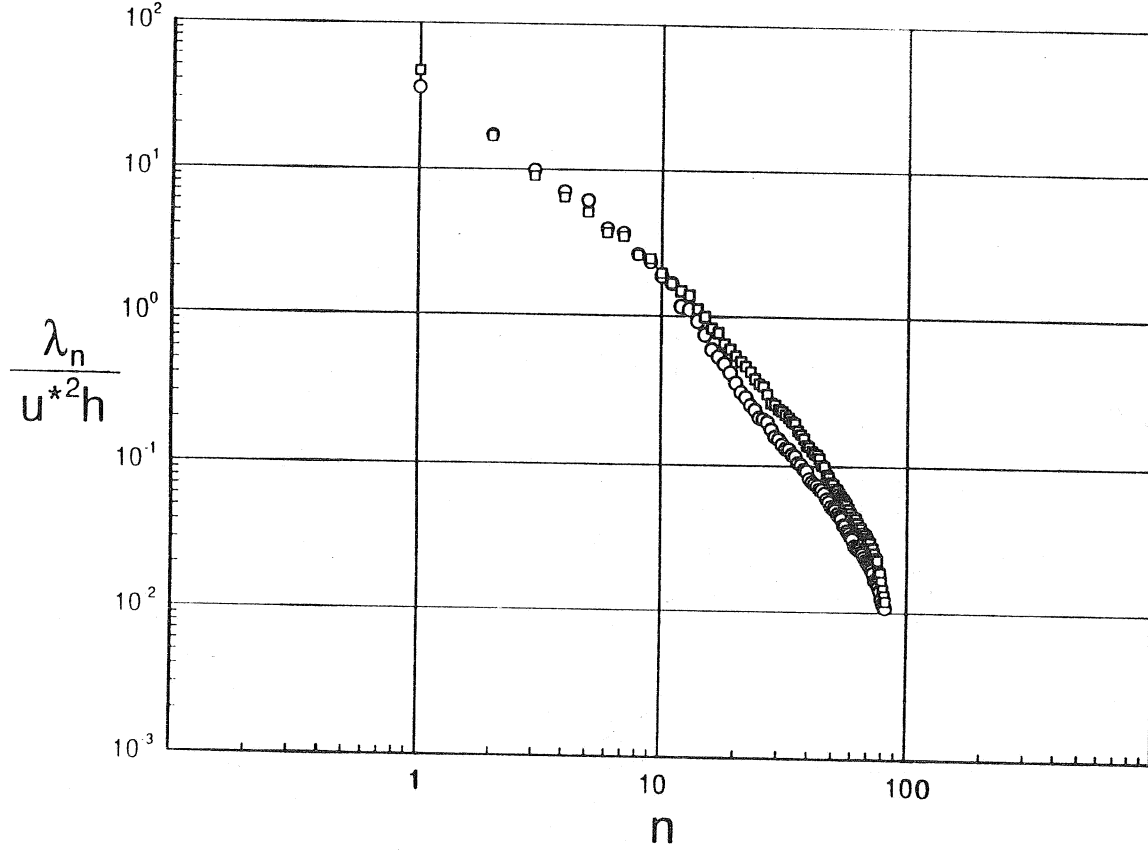


FIG. 3. Eigenvalue spectra of the 1-D POD of turbulent channel flow at $Re_h = 5,378$ (circles), 29,935 (squares). The decomposition domain is $0 \leq y \leq h$.

profile are 1120 for the boundary layer and 543 for the $Re_h = 5,378$ channel flow. For purposes of comparison the eigenvalue problem has been recomputed on a domain extending from the wall up to $y^+ = 130$, the upper limit of Lu and Smith's data. The non-dimensional eigenvalue spectra in Fig. 4 agree very well. The eigenfunctions display some differences in the amplitudes of their oscillations, but these may be due to noise in the correlation data. A more fundamental property of the eigenfunctions, the locations of the zeroes, behaves almost identically for both flows. The patterns of the locations of the zeroes of each of the modal orders (see the inset of Fig. 4) are remarkably similar. While universality of the outer law for the POD will require further proof, the similarity between the boundary layer flow and the channel flow is very suggestive.

In summary, in the outer region of wall turbulence the eigenfunctions and eigenvalues of the POD have been shown to be similar when scaled by outer variables. The similarity extends over different Reynolds numbers and different flows. One may view this similarity as a generalization of the classical law of the wall to the POD. The similarity significantly simplifies the representation of turbulence by POD, and makes it feasible to apply the POD decomposition more widely.

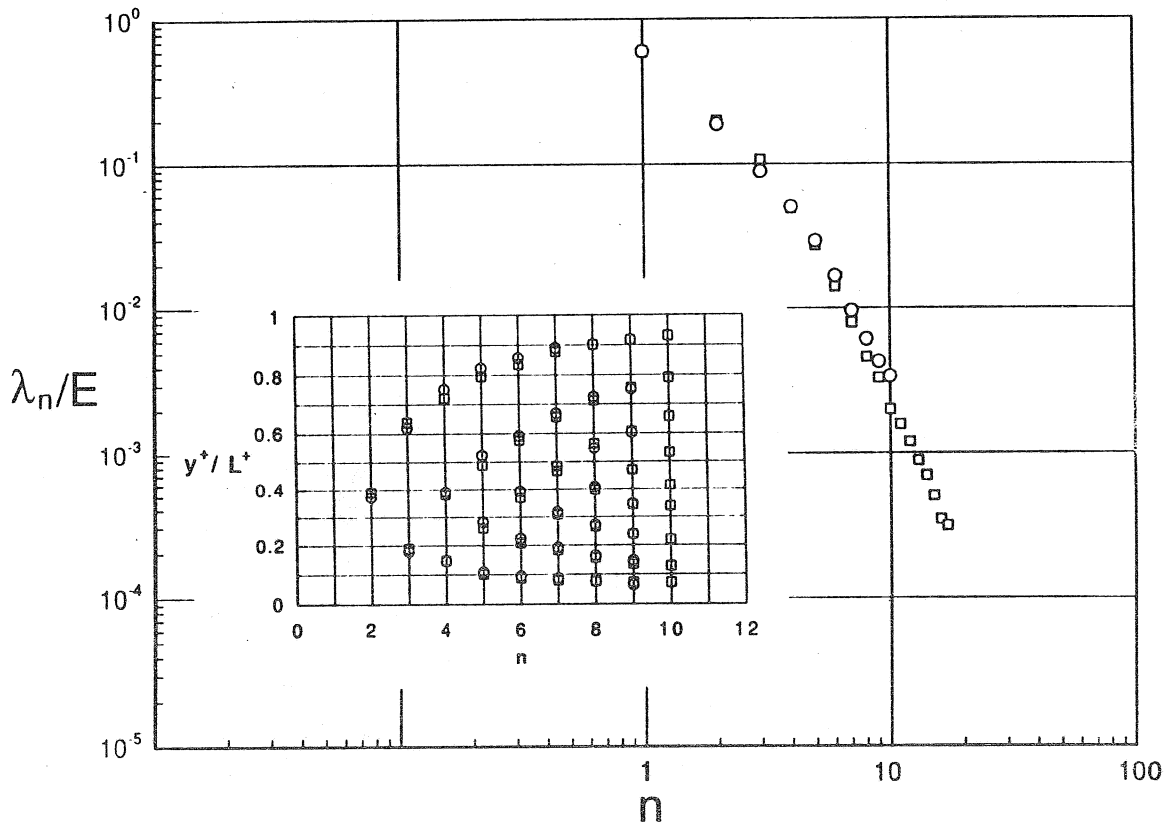


FIG. 4. Eigenvalue spectra of turbulent channel flow (squares) at $Re_h = 5,378$ and turbulent boundary layer (circles) at $Re_\theta = 1120$ (Lu & Smith¹⁴). The domain of the decomposition is $0 < y^+ < 130$ in each case. The insert shows zero crossings of eigenfunctions up to order of 9 for the two cases. The zero locations in the inhomogeneous normal direction are normalized by $L^+ = 130$.

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